

Modelling tools & applications

ICAS-MoT

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Overview

Modelling concept (summary)
Tool for model analysis & solution (MoT)
Examples with MoT



Modelling concept - 1

For a given modelling task, generate (create) the mathematical model; analyze the model; solve the model; create a model object & finally use





Modelling concept - 2

For a given modelling task, generate (create) the mathematical model; analyze the model; solve the model; create a model object & finally use





Tool for model generation: ModDev -1 Describe balance volume (control shell) & connection to surroundings; retrieve equations from model library; export model to MoT



Tool for model generation: ModDev -2 Describe balance volume (control shell) & connection to surroundings; retrieve equations from model library; export model to MoT



Tool for model generation: ModDev -3 Describe balance volume (control shell) & connection to surroundings; retrieve equations from model library; export model to MoT



Match problem description with Reference Models



Can be transferred into balance equations for other extensive quantities by symbolic manipulation

Retrieve matched models otherwise build new models

9

PSE for SPEED for model generation: ModDev - example



STREAM CONNECTION OBJECT Name: 3 Models for quantities: Energy (enthalpy): $H_3 = @FUNC_E(2,f_{3[]},T_3,P_3)$ Models for the "from"-connection: (equilibrium) Energy connection: $T_3 = T_{flash}$ Momentum connection: $P_3 = P_{flash}$

SHELL OBJECT

Name: *flash* Assumed phase condition: *Calculate* (*VL*) Equilibrium model: $0 = f_{2i}/ft_2 - K_{flash} * f_{3i}/ft_3$, @KEQ(T_{flash}, P_{flash} , $f_{2[]}, f_{3[]}, \#K_{flash}$), no accumulation, include mass & energy balance

SHELL CONNECTION OBJECT Name: *heater* Connection models: Energy connection: $Q_{heater} = Q_{flash}$

PSE for model generation: ModDev - example

```
Tl = Tout
Pl = Pout
Ttank=Tout
Tv = Tl
Pv = Pl
ntot = sum_i(n[i])
zTank[i] = n[i]/ntot
```

Model equations written in ASCII-text is exported to MoT

```
#find k values
    Psat[i] = (10<sup>^</sup>(DB AntoineA[i] - DB_AntoineB[i]/(Tout-273.15+DB_AntoineC[i]) ))/760
    K[i] = Psat[i]/Pout
    x[i] = zTank[i] / (1+phi*(K[i]-1))
    y[i] = x[i] *K[i]
                                   #get the densities
    #get the enthalpies
    #hVap[i] = (Avap[i]*(1-(Tout/'
                                   #dL[i] = A105[i]/B105[i]^(1+(1-Ttank/C105[i])^D105[i])
                                   dL[i] = ADippr101[i]/BDippr101[i]^(1+(1-Ttank/CDippr101[i])^DDippr101[i])
    #hV[i]=(((((E[i]*0.2*Tout+D[i]
    #hVr[i]=(((((E[i]*0.2*Tref+D[:
    #hL[i] = (((((E[i]*0.2*Tout+D] DenL = 1 / sum i( x[i]/dL[i] )
    #hLr[i] = (((((E[i]*0.2*Tref+I DenV = Pout/(0.08314*Tout)
                                   #rachford rice
                                   0 = ntot*(1-phi)/DenL + ntot*phi/DenV - Vol
                                   0 = sum i( zTank[i]*(1-K[i]) / (1 + phi*(K[i]-1)) )
Note: all the
                                   Level = ntot*(1-phi)/(Area*DenL)
                                   L = ValveL*Level
model
                                   V = ValveV*(Pout-Pmin)
                                   Hv = sum i((hV[i]-hVr[i]+hVap[i])*y[i])
                                   Hl = sum i( (hL[i]-hLr[i])*x[i] )
equations are
                                   0 = (Hl*ntot*(1-phi) + Hv*ntot*phi - Htank)/1000
not shown here
                                   #update holdups
                                   dndt[i] = F^{*}z[i] - L^{*}x[i] - V^{*}y[i]
                                   dHtankdt = Hf*F - Hl*L - Hv*V + q
```

Tool for model analysis & solution: MoT

| 🞽 MoT | | |
|--|---|---|
| File Edit View Window Help | Translated form of t | he model |
| Model Definition Wiew Original Model View Translated Model Modify Model Variable Analysis Classify Variables Define Relationships Show Equation and Va Set Variable Value Model Def | hLFeed[i] = (((([E[i]*0.2*Tfeed+D[i]*0.25)*Tfeed+C[i]/3.0)*T Hv = sum_i((hV[i]-hVr[i])*y[i]) HI = sum_i((hL[i]-hLr[i])*x[i]) Hf = sum_i((hLFeed[i]-hLr[i])*z[i]) ntot = sum_i(n[i]) zTank[i] = n[i]/ntot dL[i] = A105[i]/B105[i]^(1+(1-Ttank/C105[i])^D105[i]) DenL = sum_i(x[i]*dL[i]) DenV = Pout/(0.08314*Tout) O = ntot*(1-phi)/DenL + ntot*phi/DenV - Vol 0 = sum_i(zTank[i]*(1-K[i]) / (1 + phi*(K[i]-1))) 0 = HI*ntot*(1-phi) + Hv*ntot*phi - Htank Level = ntot*(1-phi)/(Area*DenL) L = ValveL*Level V = ValveV*(Pout-Pmin) dndt[i] = F*z[i]-L*x[i]-V*y[i] dHtankdt = Hf*F - HI*L - Hv*V + q | feed+B[i]*0.5)*Tfeed+A[i])*Tfeed)/1 Library Explicit Implicit ODE |
| ==> Translator says: Model imp Modelling Testbed ver. 0.1 Init Complete | oorted succesfully. .ocal Variable View) Variable Chart Trace / | |
| Heady | Model: 1 JEQ's: 18 JUnknown: U JU | /eg. of Freedom: 3 Y: U dY/dt: U 🥥 ⊖dr/suit = 12·02 |
| Microsoft Visual C++ Runtime | MoT | ≈7 ⁻ ∎ ₩√(-12.02 |

Tool for model analysis & solution: MoT





| Eq. No. | Equation | Numberof | | | |
|---|---|-----------|--|--|--|
| | | equations | | | |
| 1 | $\ln q_i = b_n (Z - 1) - \ln(Z - B) - A/B (2a_n^{0.5} - b_n) \ln(1 + B/Z) \qquad i = 1, NC$ | NC | | | |
| 2 | $a_{n} = (\alpha_{n}^{0.5} \Gamma_{n} / P_{n}^{0.5}) / \sum_{i} (x_{i} \alpha_{j}^{0.5} \Gamma_{n} / P_{n}^{0.5}) \qquad i=1, NC$ | MC | | | |
| 3 | $b_n = (T_n/P_n)/\sum_j (x_j, T_q/P_q) \qquad i=1, NC$ | MC | | | |
| 4 | $Z^{2} - Z^{2} + Z(A - B - B^{2}) - AB = 0$ | 1 | | | |
| 5 | $A = aP(RI)^2$ | 1 | | | |
| 6 | B = bP(RI) | 1 | | | |
| 7 | $a = \sum_{i} x_i \sum_{j} x_j a_{ij} \qquad i=1, NC; j=1, NC$ | 1 | | | |
| 8 | $b = \sum_{i} x_i x_j b_{ij} \qquad i=1, NC; j=1, NC$ | 1 | | | |
| 9 | $a_{ij} = (a_i a_j)^{k} (1 - k_{ij})$ $i = 1, NC_i j = 1, NC$ | MC*MC | | | |
| 10 | $b_{ij} = (b_i + b_j)/2$ $i=1, NC; j=1, NC$ | MC*MC | | | |
| 11 | $a_i = \psi_A \alpha_i (T) (R^2 T_n^2 / P_n) \qquad i=1, NC$ | NC | | | |
| 12 | $b_i = \psi_B(RT_n/P_n) \qquad i=1, NC$ | MC | | | |
| 13 | $\alpha_{i}(T) = [1 + m_{i}(1 - T_{h}^{0.5})]^{2} \qquad i = 1, NC$ | MC | | | |
| 14 | $m_i = 0.48 \pm 1.574 \omega_i - 0.176 \omega_i^2$ $i=1, NC$ | MC | | | |
| μs | $T_{ib} = T/T_{ib} \qquad i=1, NC$ | MC | | | |
| Total number of equations = 5 + 8NC + 2NC*NC | | | | | |
| Total number of variables = 10 [T, P, R, ψ_{A} , ψ_{B} , a, b, A, B, Z] + 12NC [x, T _o , P _o , a) T _B α | | | | | |
| $\underline{m} \ \underline{a}, \ \underline{b}, \ \underline{a}, \ \underline{b}, \ \underline{p}] + 3NC^*NC[\underline{a}, \ \underline{b}, \ \underline{k}] = 10 + 12NC + 3NC^*NC$ | | | | | |



Table 2d: Incidence matrix of SRK EOS property model equations.

| T | Unknown Variables | | | | | | | | | | | | | | |
|----------------|-------------------|---|---|---|----------|----------|----------|---|---|---|---|---|-----------------------|----|---|
| Eq. | Tr | т | α | b | <u>a</u> | <u>b</u> | <u>a</u> | а | Ь | В | Α | Ζ | <u>b</u> _y | ₫y | Ø |
| 15 | * | | | | | | | | | | | | | | |
| 14 | | * | | | | | | | | | | | | | |
| 13 | * | * | * | | | | | | | | | | | | |
| 12 | | | | * | | | | | | | | | | | |
| 11 | | | * | | * | | | | | | | | | | |
| 10 | | | | * | | * | | | | | | | | | |
| 9 | | | | | * | | * | | | | | | | | |
| 7 | | | | | | | * | * | | | | | | | |
| 8 | | | | | | * | | | * | | | | | | |
| 6 | | | | | | | | | * | * | | | | | |
| 5 | | | | | | | | * | | | * | | | | |
| 4 ¹ | | | | | | | | | | * | * | * | | | |
| 3 | | | | | | | | | | | | | * | | |
| 2 | | | * | | | | | | | | | | | * | |
| 1 | | | | | | | | | | * | * | * | * | * | * |

¹: requires the solution of a cubic equation in Z

Tool for model analysis & solution: MoT

| | Brook | Equation | Doputt |
|--------------------------|-------|--|---------------------------------------|
| | | C=VON | n n n n n n n n n n n n n n n n n n n |
| | | E=VEM | 0 0 |
| Solver Options | | | 25 |
| 📋 Solution Options | 4 | dV=Fin-Fout | 0 |
| 🔤 Variable Bounds | 5 6 | option2=qGmax | 0.02 |
| Stepwise Model Solution | 6 | qO2lim=qO2max | 0.00657 |
| | 7 | Gm=G/MwG | 0 |
| | 8 | Em=EMWE | 0 |
| Misc | 9 | qGoxlim=qO2lim/kog | 0.00285652 |
| 👘 📋 Variable Chart Trace | 10 | EPR=Em*kla*air | 0 |
| 📕 Show Solution | 11 | option1=qG0m+alpha*(Gm-G0m) | 0.001325 |
| | 12 | qEmpot=gamma*Em | 0 |
| I | 13 | option4=qGoxlim | 0.00285652 |
| I | 14 | qGm=min(option1,option2) | 0.001325 |
| I | 15 | option5=qEmpot | 0 |
| I | 16 | qG=MwG*qGm | 0.2385 |
| I | 17 | option3=qGm | 0.001325 |
| I | 18 | dVG=-qG*VX+Gin*Fin-G*Fout | 27.615 |
| I | 19 | qGr=min(option3,option4) | |
| I | 20 | qGf=max(qGm-qGr,0) | |
| I | 21 | option7=(qO2lim-kog*qGr)/koe | |
| I | 22 | qEoxlim=max(option7,0) | |
| I | 23 | option6=qEoxlim | |
| I | 24 | qEr=min(option5,option6) | |
| I | 25 | qEm=-qEr+keg*qGf | |
| | 26 | qCO2=kc1*qGr+kc2*qGf+kc3*qEr | |
| | | | |
| | | mum=YGr*qGr+YGt*qGf+YEr*qEr | |
| ng Defi 📲 🛱 Sol 📲 🛱 Opti | 29 | dQspec=(dQGr*qGr+dQGf*qGf+dQEr*qEr)/3600 | |

0.001325 option3 option4 0.00285652173913

Status λ Variable View λ Local Variable View \bigwedge Variable Chart Trace j

qGr

L E L MI



Tool for model analysis & solution: MoT Select the appropriate solver options

| Verify Model Solution Options | | | | | | |
|--|---|--|--|--|--|--|
| Overall Solution Selection | Algebraic Options Dynamic Options Optimizer Options | | | | | |
| Function Evaluation Unly Dynamic Solution | Dynamic Solver BDF Bunge-Kutta (5th order) | Integration Options Forward Backward | | | | |
| Model Ordering Options | | Forward then backward Backward then forward | | | | |
| Ordered Partitioned and Ordered | Number of time 300 steps | Generate eigenvalue repo | | | | |
| | Model scaling 1 | Hun to steady state Steady state solution | | | | |
| Specify multiple runs | Global error control (eps) | Criteria 1e-006 | | | | |
| Solve Abort | | | | | | |







Use of MoT model-objects

- Run MoT models on a stand-alone basis
- Run MoT models from a simulator (export MoT models to ICAS or other simulation engines)
- Run Mot models from external software environments (for example, EXCEL)
- Create customized simulator!



Modelling exercise – MoT

Run MoT model objects from EXCEL

Note: It is necessary to first execute ComMOT.exe and then open the supplied EXCEL-macro (MoT_Model_Interface.xls)